

# *Long Island Sound Nitrogen Removal Training Program*

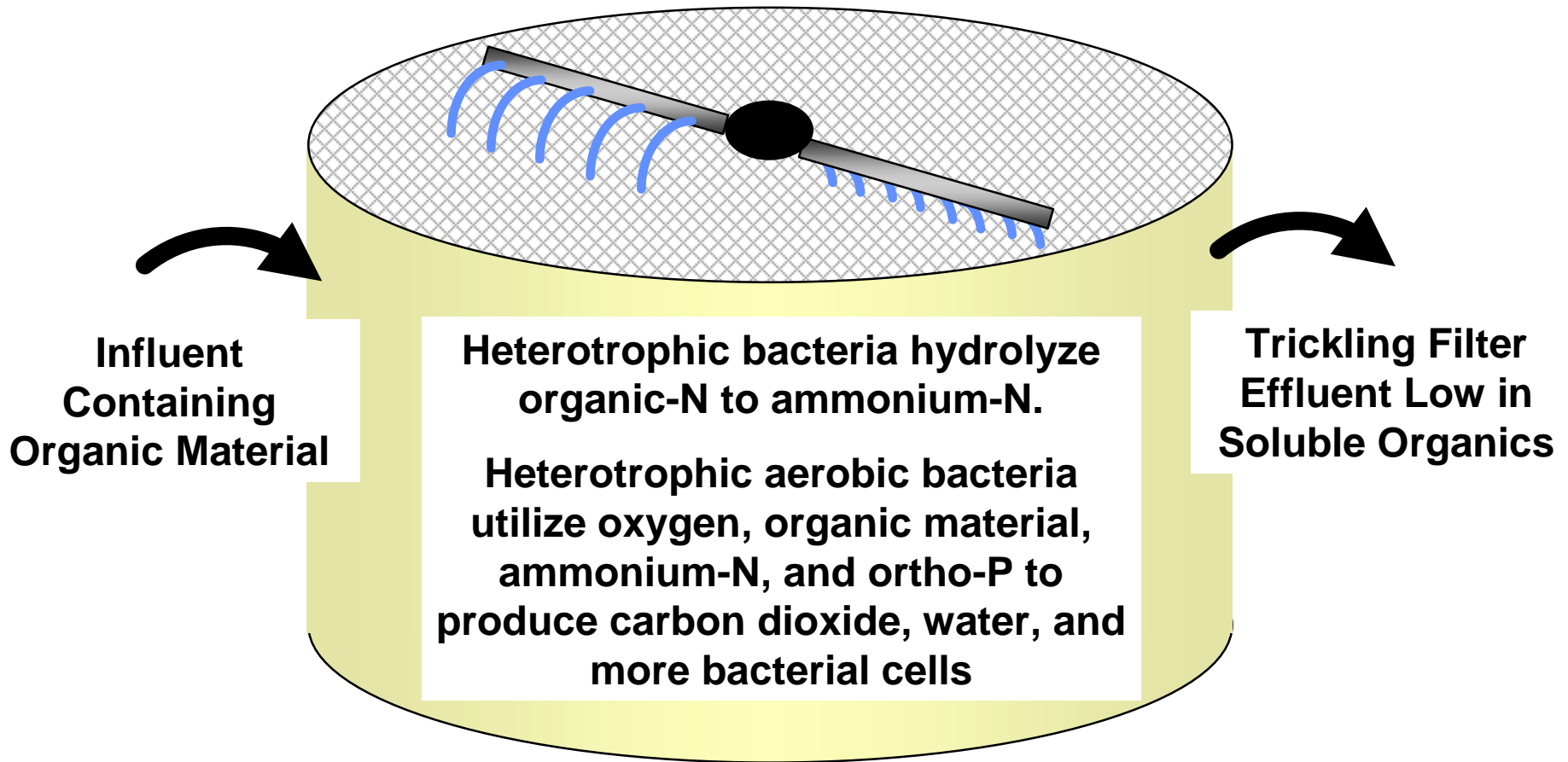
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## *Module 4 Fixed Film Operational Strategies*

**SUNY Farmingdale  
February 12 & 13, 1997**



# *BOD Removal in Fixed Film Processes*



# *Nitrification*



Oxygen Required = 3.43 lb / lb N oxidized

Alkalinity Required = 7.14 lb as CaCO<sub>3</sub> / lb N oxidized



Oxygen Required = 1.14 lb / lb N oxidized

For both reactions together:

Total Oxygen Requirement = 4.57 lbs / lb N oxidized

Total Alkalinity Requirement = 7.14 lbs as CaCO<sub>3</sub> / lb N oxidized



# *Factors Affecting Nitrification*

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## **What Factors Affect Nitrification in Fixed Film Processes**



# *Factors Affecting Nitrification in Fixed Film Processes*

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- **BOD loading rate**
- **Ammonia loading rate**
  - Per unit surface area
  - Per unit volume
- **Dissolved oxygen**
- **Hydraulic loading rate**
- **Recirculation**
- **Temperature**
- **pH**
- **Alkalinity**
- **Inhibitory compounds**
- **Predator growth**



# *BOD Loading Rates for Carbonaceous BOD Removal in the Trickling Filter or RBC Process*

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- **Trickling Filter Loading Rate**
  - 25 lbs BOD<sub>5</sub> / day / 1000 cu ft (rock media)
  - 1.7 lbs BOD<sub>5</sub> / day / 1000 sq. ft.
- **RBC Loading Rate**
  - 1.0 to 2.0 lbs / day / 1000 sq. ft.



# *BOD Loading Rates for Nitrification in the Trickling Filter or RBC Process*

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- **Trickling Filter Loading Rate**
  - 5 lbs BOD<sub>5</sub> / day / 1000 cu ft (rock media)
  - 0.3 lbs BOD<sub>5</sub> / day / 1000 sq. ft.
- **RBC Loading Rate**
  - 0.8 lbs BOD<sub>5</sub> / day / 1000 sq. ft.



# *Definitions*

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**Heterotroph** - Organism which uses organic matter for energy and growth. The BOD-removers and denitrifiers in BNR systems are heterotrophic organisms

**Autotroph** - Organism which uses inorganic matter for energy and growth. The nitrifiers in BNR systems (nitrosomonas and nitrobacter) are autotrophic organisms





# *Competition Between Heterotrophs and Autotrophs*

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- **Heterotrophs (BOD-removers) have competitive advantage over autotrophs (nitrifiers)**
- **Heterotrophs grow at head end of TF or RBC, autotrophs grow at tail end**
- **Soluble BOD<sub>5</sub> must drop below about 15 mg/L to allow nitrifiers to grow**



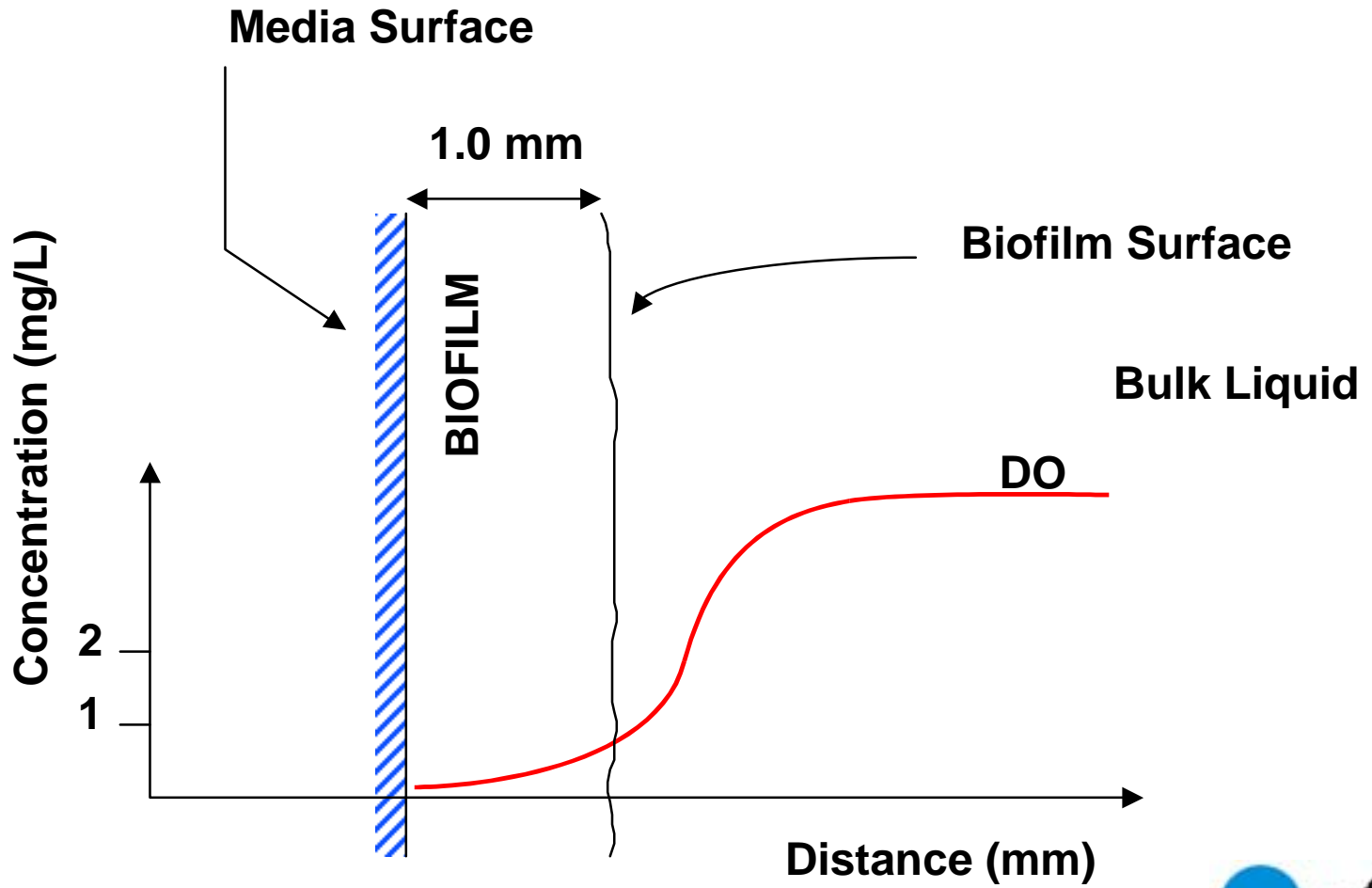
# *Dissolved Oxygen*

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- **As dissolved oxygen increases, nitrifier growth rate increases**
- **Oxygen available to nitrifiers is affected by turbulence and diffusion into biofilm**
- **DO concentration often masks pH and temperature effects**
- **At temperatures above 15°C dissolved oxygen is often the rate limiting parameter**
- **Forced ventilation for TFs or aerated RBCs can increase nitrification rate**



# *DO Depletion in Biofilm*



# *Hydraulic Loading Rate - Trickling Filters*

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- **Typical 25 - 200 gpd per sq. ft. of trickling filter plan area**
- **Past studies indicated importance of recirculation rate in Trickling Filters**
- **More recent studies have indicated no significant benefit from recirculation as long as sufficient wetting is provided**
- **Use 1:1 recirculation directly around trickling filter**
- **Some studies have shown benefits from slowing down distributor, other studies have shown no benefit to slowing distributor**



# *SK Approach*

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$$SK = \frac{(Q+R)(1.337 \times 10^5 \text{ cu. ft./mil.gal.})(304.8 \text{ mm/ft})}{(A)(a)(n)(1440 \text{ min/d})}$$

**SK = flushing intensity, mm/pass of an arm**

**Q+R = average flow to trickling filters, mgd**

**A = total trickling filter plan area, sq. ft.**

**a = number of arms**

**n = rpm**



# *Suggested SK Values*

<b><u>BOD5 loading (lb/d/1000 cu.ft.)</u></b>	<b><u>Design SK mm/pass</u></b>	<b><u>Flushing SK mm/pass</u></b>
<b>16</b>	<b>10-100</b>	<b>&gt;200</b>
<b>31</b>	<b>15-150</b>	<b>&gt;200</b>
<b>62</b>	<b>30-200</b>	<b>&gt;300</b>
<b>125</b>	<b>40-250</b>	<b>&gt;400</b>
<b>187</b>	<b>60-300</b>	<b>&gt;600</b>
<b>250</b>	<b>80-400</b>	<b>&gt;800</b>

Adapted from WEF MOP 8, 1992, p. 697, Table 12.4



# *Hydraulic Loading Rate - RBCs*

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- **Typical 1 - 3 gpd per sq. ft. of media surface area**
- **Recirculation is not normally necessary in RBC systems**
- **In aerated RBCs or SBCs, can provide a return sludge stream and develop some suspended growth in RBC basin**
- **Recirculation of RBC effluent in nitrifying systems may provide some denitrification**



# *Competing Effects of Increasing Temperature*

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## **Increases BOD Uptake Rate**

- Reduces BOD in Bulk Phase
- *Increases Nitrification Rate*

## **Increases Nitrifier Growth Rate**

- *Increases Nitrification Rate*

## **Decreases Solubility of Oxygen in Water**

- Reduces Oxygen Transfer into Biofilm for Same Air Flow
- *Decreases Nitrification Rate Unless Air Flow Rate Increased*

**Result - Often no temperature effect is observed  
between 15°C and 20°C**



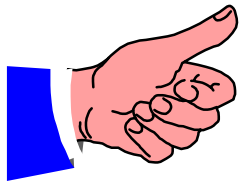


# *Effect of pH and Alkalinity on Nitrification*

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**Nitrification consumes alkalinity and lowers pH of the wastewater**

**pH below 6.5 or above 8.0 can significantly inhibit nitrification.**



## **Rules of Thumb:**

**Maintain pH in the range 6.5 - 8.0 for optimum nitrification.**

**Overall alkalinity consumption is generally less than the theoretical 7.14 lbs as  $\text{CaCO}_3$  per lb of ammonia-N nitrified.**



# *Simplified Calculation of Alkalinity Requirement for Nitrification*

**Given:**

$$\begin{aligned}\text{Plant Influent Flow} &= 10 \text{ mgd} \\ \text{Primary Effluent TKN} &= 31.5 \text{ mg/l}\end{aligned}$$

**Alkalinity Consumed by Nitrification :**

**In lbs/day**

$$\begin{aligned}(10) \text{ mgd} & \times (31.5 \text{ mg/l}) & \times (7.14) & \times (8.34) & = & 18,757 \text{ lbs alkalinity} \\ \text{Flow} & \text{TKN conc.} & \text{lbs. of alkalinity} & & & \text{as CaCO}_3 \text{ per day} \\ (\text{mgd}) & (\text{mg/l}) & \text{required per lb of} & & & \\ & & \text{ammonia-N nitrified} & & & \end{aligned}$$

**In mg/l**

$$(31.5 \text{ mg/l}) \times (7.14) = 225 \text{ mg/l alkalinity as CaCO}_3 \text{ consumed}$$



# Sources of Alkalinity

Source	Form Delivered	lbs. Alkalinity as CaCO <sub>3</sub> per lb. or gallon of Product	Cost per lb. of Alkalinity as CaCO <sub>3</sub>
<b>Hydrated Lime</b>	50 lb. Bags	1.33 per lb.	\$0.074 (50 lb. Bag)
	20 Ton Truck		\$0.05 (20 Ton Truck)
<b>Sodium Bicarbonate</b>	50 lb. Bags	1.19 per lb.	\$0.36
<b>Sodium Hydroxide (Caustic Soda)</b>	55 Gallon Drum	7.87 per gallon	\$0.19 (55 Gallon Drum)
	½ Truck (1,750 Gallons)		\$0.125 (½ Truck)
	Full Truck (3,500 Gallons)		\$0.104 (Full Truck)

Module:  
Unit:  
Transparency:



# *Compounds Which Inhibit Nitrification*

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## Organic Compounds:

Acetone

Carbon Disulfide

Chloroform

Ethanol

Monoethanolamine

Phenol

Ethylenediamine

Hexamethylene Diamine

Aniline

## Metals and Inorganic Compounds:

Zinc

Free Cyanide

Perchlorate

Copper

Mercury

Chromium

Nickel

Silver

Cobalt

Thiocyanate

Sodium Cyanide

Sodium Azide

Hydrazine

Sodium Cyanate

Potassium Chromate

Cadmium

Arsenic (trivalent)

Fluoride

Lead



# Denitrification

Nitrate + Methanol  $\longrightarrow$  Carbon Dioxide + Nitrogen Gas + Water + Hydroxide



**Methanol Utilized = 1.9 lbs methanol per lb nitrate-N denitrified**

**This is equivalent to 2.86 lbs COD utilized per lb nitrate-N denitrified**

**Alkalinity produced = 3.57 lbs as CaCO<sub>3</sub> per lb nitrate-N denitrified**



**Oxygen recovered = 2.86 lbs per lb nitrate-N denitrified**



# *Simplified Calculation of Oxygen and Alkalinity Recovered by Denitrification*

**Given:**

**Plant Influent Flow = 10 mgd  
Nitrate to be Denitrified**

**Oxygen Recovered**

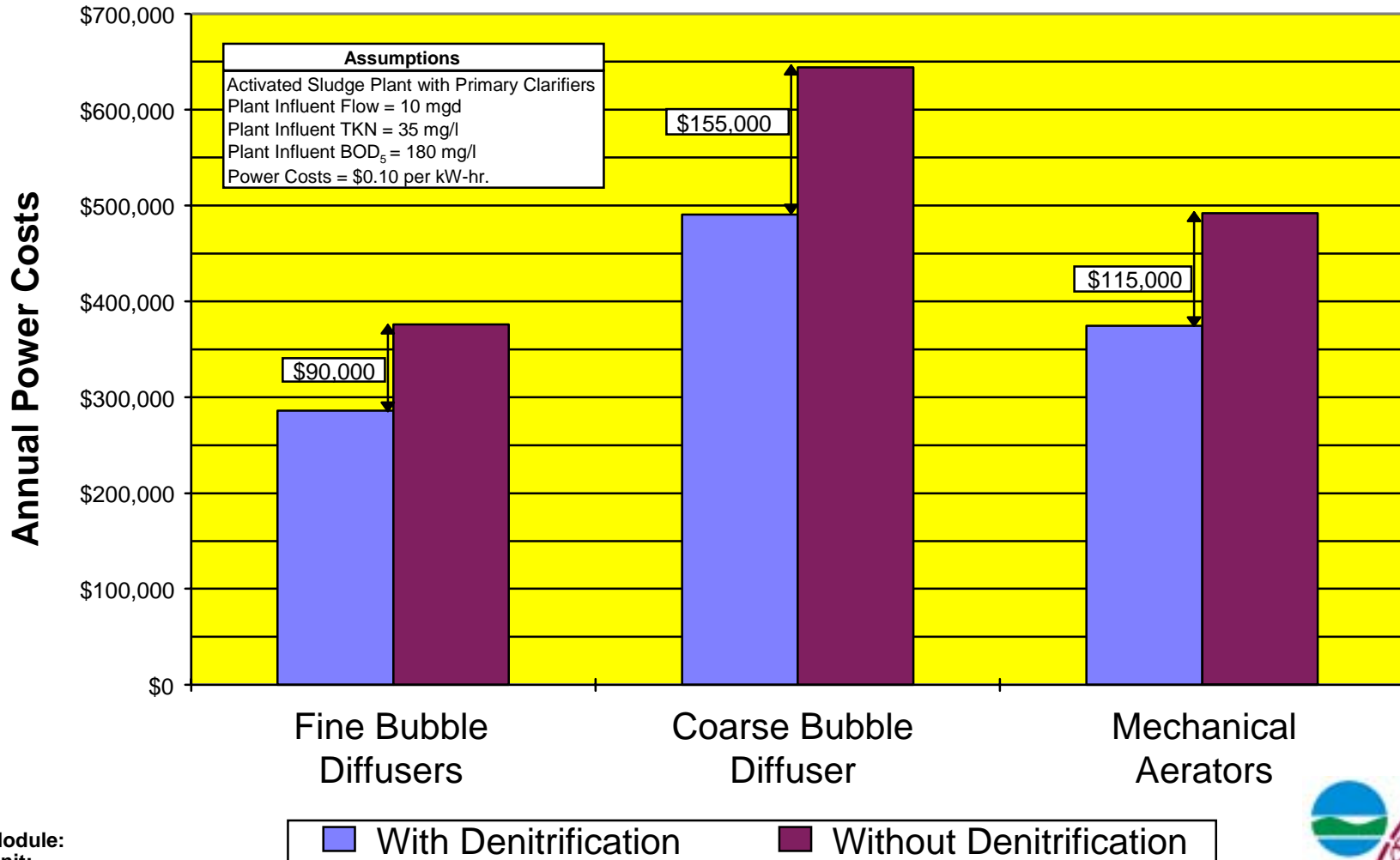
$$\begin{array}{r} \text{(10 mgd)} \\ \text{Flow} \\ \text{(mgd)} \end{array} \times \begin{array}{r} \text{(22 mg/l)} \\ \text{Nitrate-N} \\ \text{to be} \\ \text{Denitrified} \end{array} \times \begin{array}{r} 2.86 \\ \text{lbs O}_2 \\ \text{recovered} \\ \text{per lb nitrate} \\ \text{denitrified} \end{array} \times 8.34 = 5,248 \text{ lbs O}_2 \\ \text{recovered per day}$$

**Alkalinity Recovered**

$$\begin{array}{r} \text{(10 mgd)} \\ \text{Flow} \\ \text{(mgd)} \end{array} \times \begin{array}{r} \text{(22 mg/l)} \\ \text{Nitrate-N} \\ \text{Denitrified} \end{array} \times \begin{array}{r} 3.57 \\ \text{lbs alkalinity} \\ \text{per lb nitrate} \\ \text{denitrified} \end{array} \times 8.34 = 6,550 \text{ lbs alkalinity as CaCO}_3 \\ \text{recovered per day}$$



# Potential Aeration Power Savings Due to Denitrification



# *Effect of Dissolved Oxygen on Denitrification*

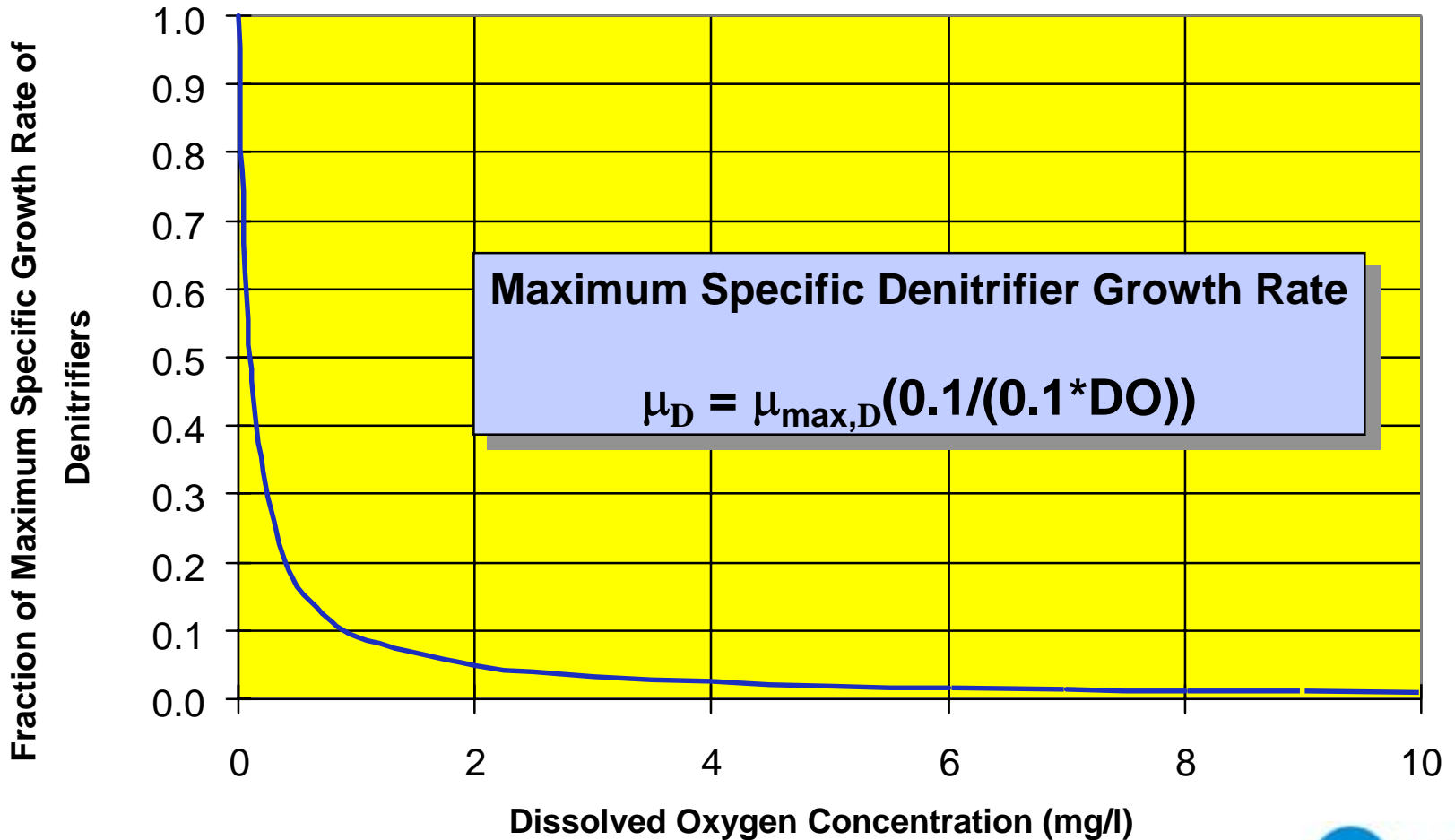
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- **Dissolved oxygen inhibits denitrification.**
- **As DO increases, denitrification rate decreases.**
- **To achieve denitrification, the nitrified wastewater must be subjected to anoxic conditions. This can happen to some extent within the biofilm.**





# *Effect of Dissolved O<sub>2</sub> on Denitrification Rate*



# *Effect of Temperature on Denitrification Rate*

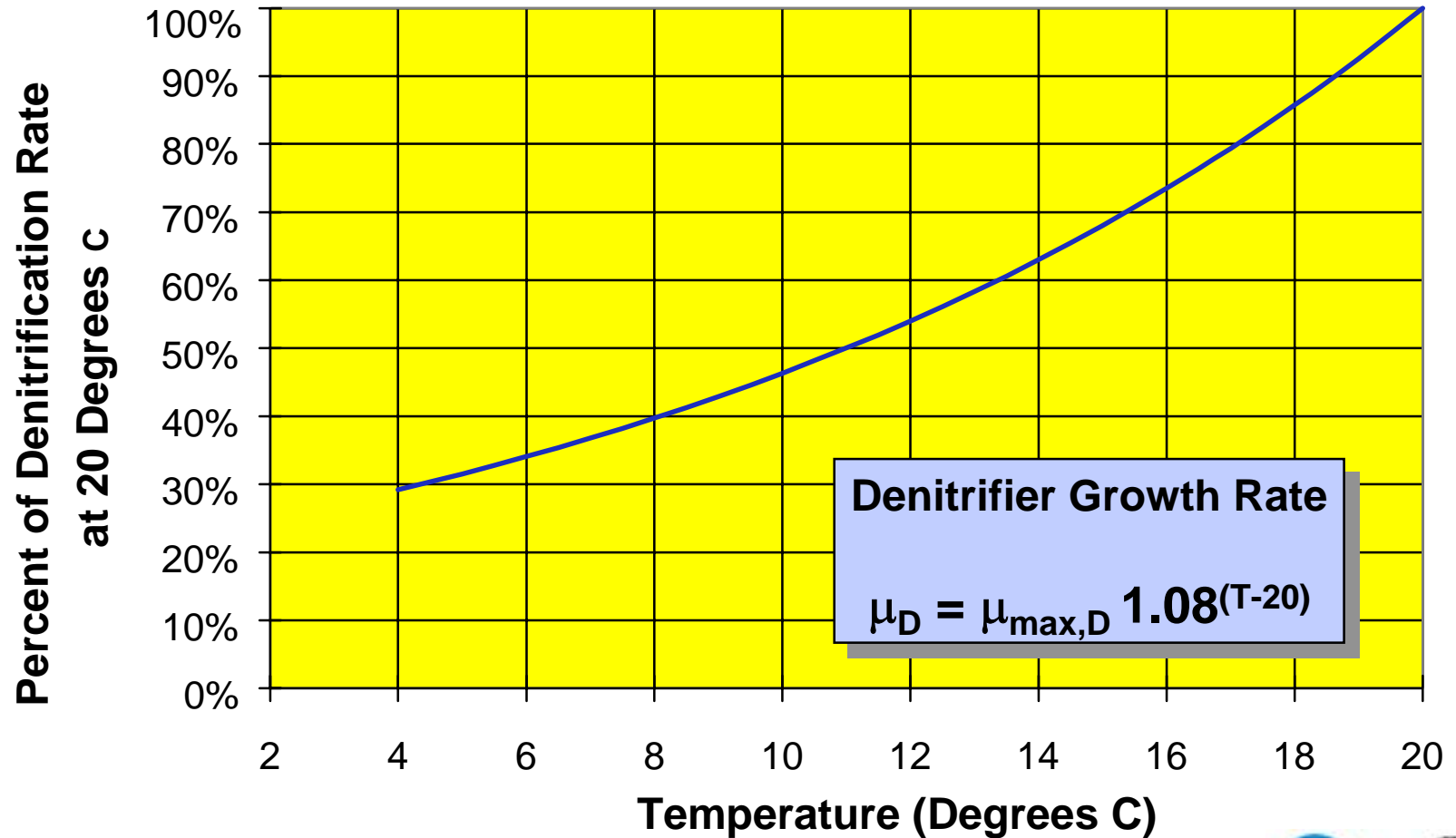
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**As temperature increases, denitrifier growth rate increases.**

**T ↑       $\mu_D$  ↑**



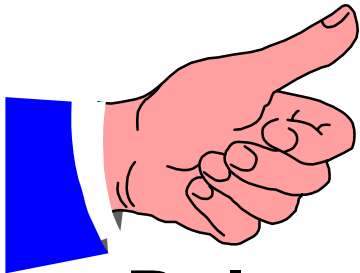
# *Effect of Temperature on Denitrification Rate*



# *Effect of pH on Denitrification Rate*

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- Denitrifiers are generally less sensitive to pH than nitrifiers.



## Rule of Thumb:

- If pH is within the recommended range of 6.5 - 8.0 for nitrification, there will be no pH effects on denitrification.



# *Effects of Inhibitory Compounds on Denitrification*

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- **Denitrifiers are generally less sensitive to inhibitory compounds than nitrifiers.**
- **If there are no compounds present which inhibit nitrification, there will probably be no inhibition of denitrification.**



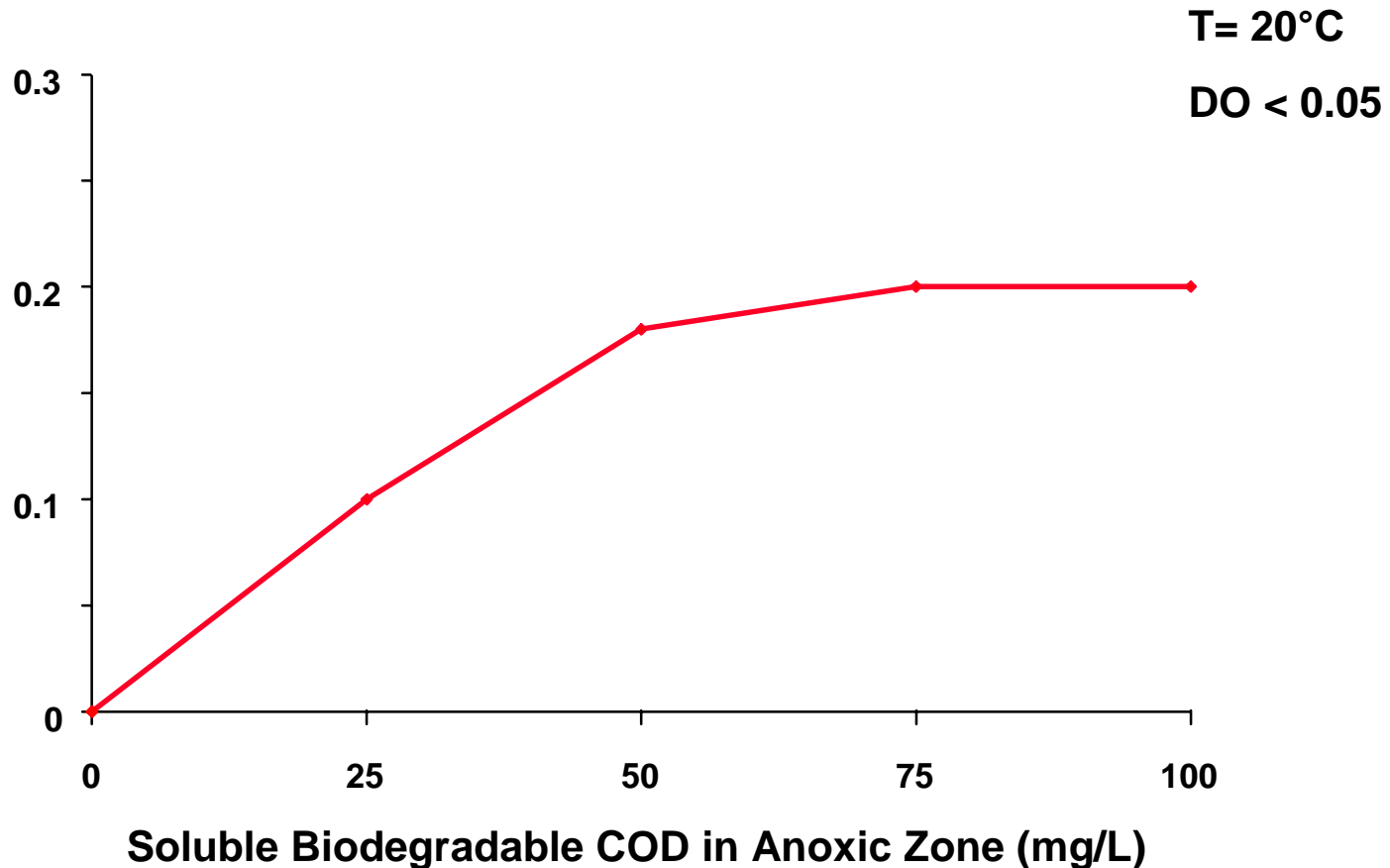
# *Effects of Available Carbon Source on Denitrification*

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- **Denitrification rate varies greatly depending upon the source of available carbon.**
  - **Highest rates are achieved with addition of an easily-assimilated carbon source such as methanol.**
  - **Lower denitrification rate is achieved with raw wastewater or primary effluent as the carbon source.**
  - **Lowest denitrification rate is observed with endogenous decay as the source of carbon.**



# *Effect of Biodegradable SCOD in Anoxic Zone on Specific Denitrification Rate*



Range of Variation of  $K_s$   
 $K_s = 20-50$  mg/L SCOD at 12°C



# *Conversion and Operation of Plants for Nitrification*

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**So, what do we need to do to  
get my plant to nitrify**





# *Conversion and Operation of Plants for Nitrification*

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**So, what do we need to do to  
get my plant to nitrify**



**Create a fixed film loading rate  
conducive to nitrification, and provide  
sufficient oxygen for nitrification**



# *Methods to Decrease Loading Rate*

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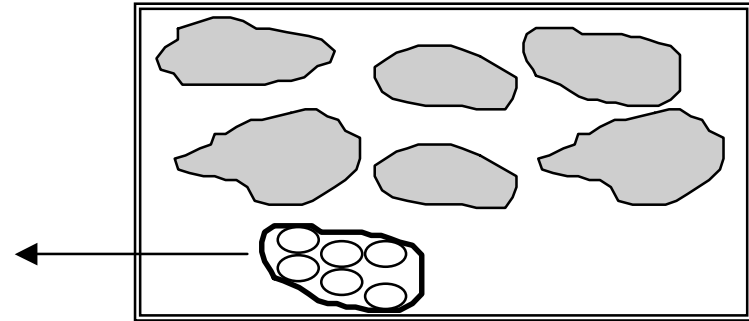
- **Activate trickling filter or RBC by adding a return sludge line**
- **Increase surface area of media in existing unit**
  - Replace rock TF media with plastic media
  - Increase RBC media density
- **Add a new biological treatment unit**
  - Tertiary trickling filter
  - Additional RBC
  - Nitrification filter



# Methods to Increase Surface Area

- Change Size of Media

Reduce Size of Media  
Increases Surface Area



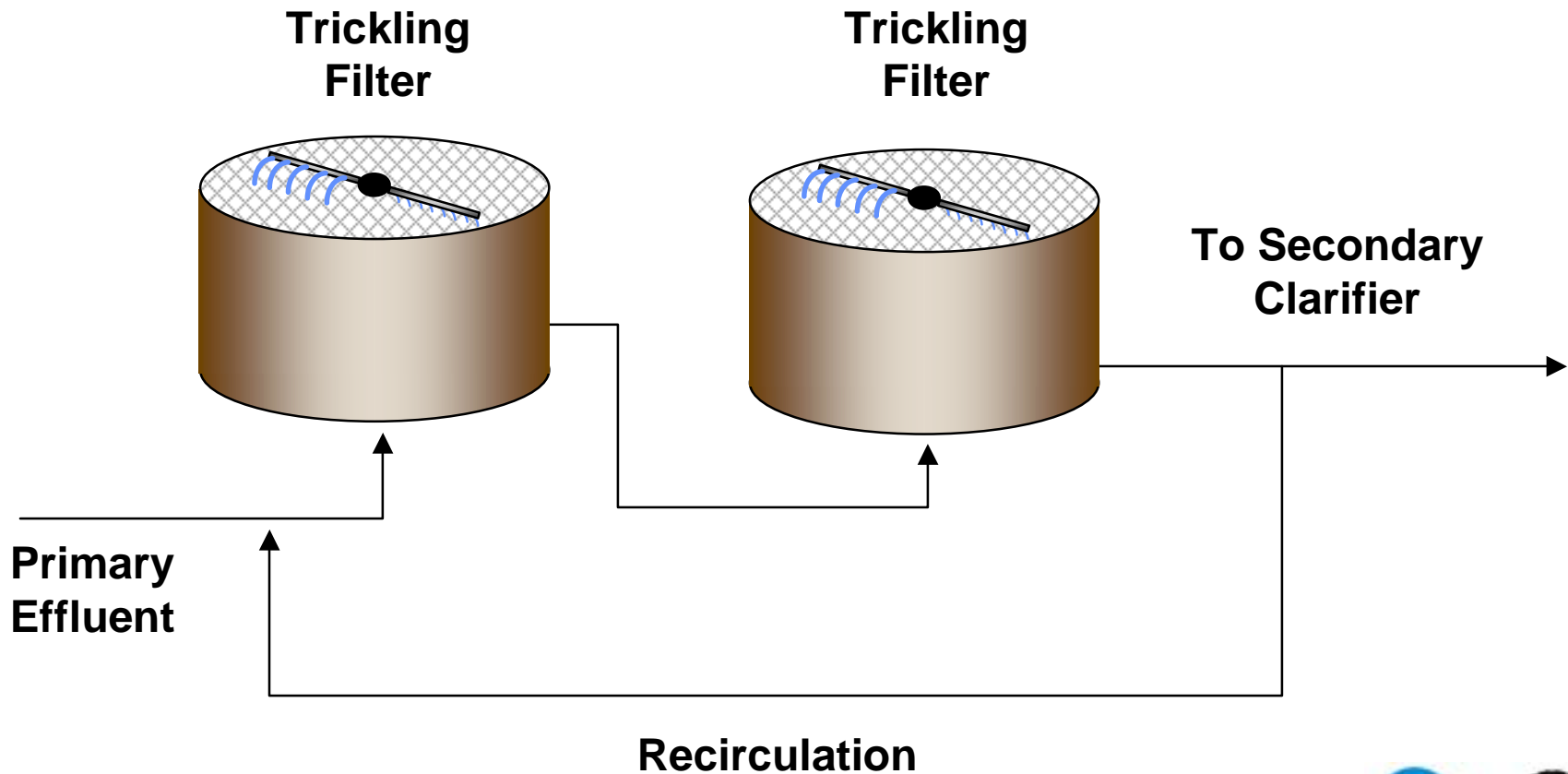
$$\text{Surface Area} \left( \frac{\text{m}^2}{\text{m}^3} \right) = \frac{\pi}{\text{DIAMETER (in m)}}$$

$$\text{Surface Area} \left( \frac{\text{ft}^2}{\text{ft}^3} \right) = \frac{\pi}{\text{DIAMETER (in feet)}}$$

**PROBLEM:** Calculate surface area per unit volume of a filter with rock media with a diameter of 150 mm (~ 6 inches) and shale with a diameter of 5 mm.

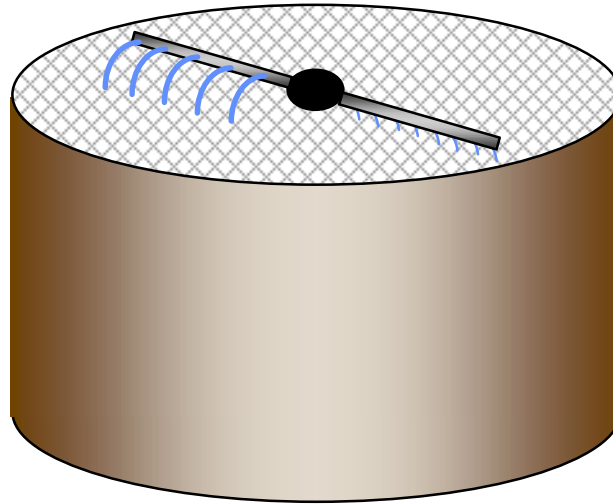


# *Convert Rock Media Trickling Filters to Plastic Media*



# *Effects of Conversion to Plastic TF Media*

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- **Higher Surface Area Per Unit Volume**
- **More Void Space - Better Oxygen Transfer**
- **Higher Volume for a Footprint -Taller Filters, Lighter Media**

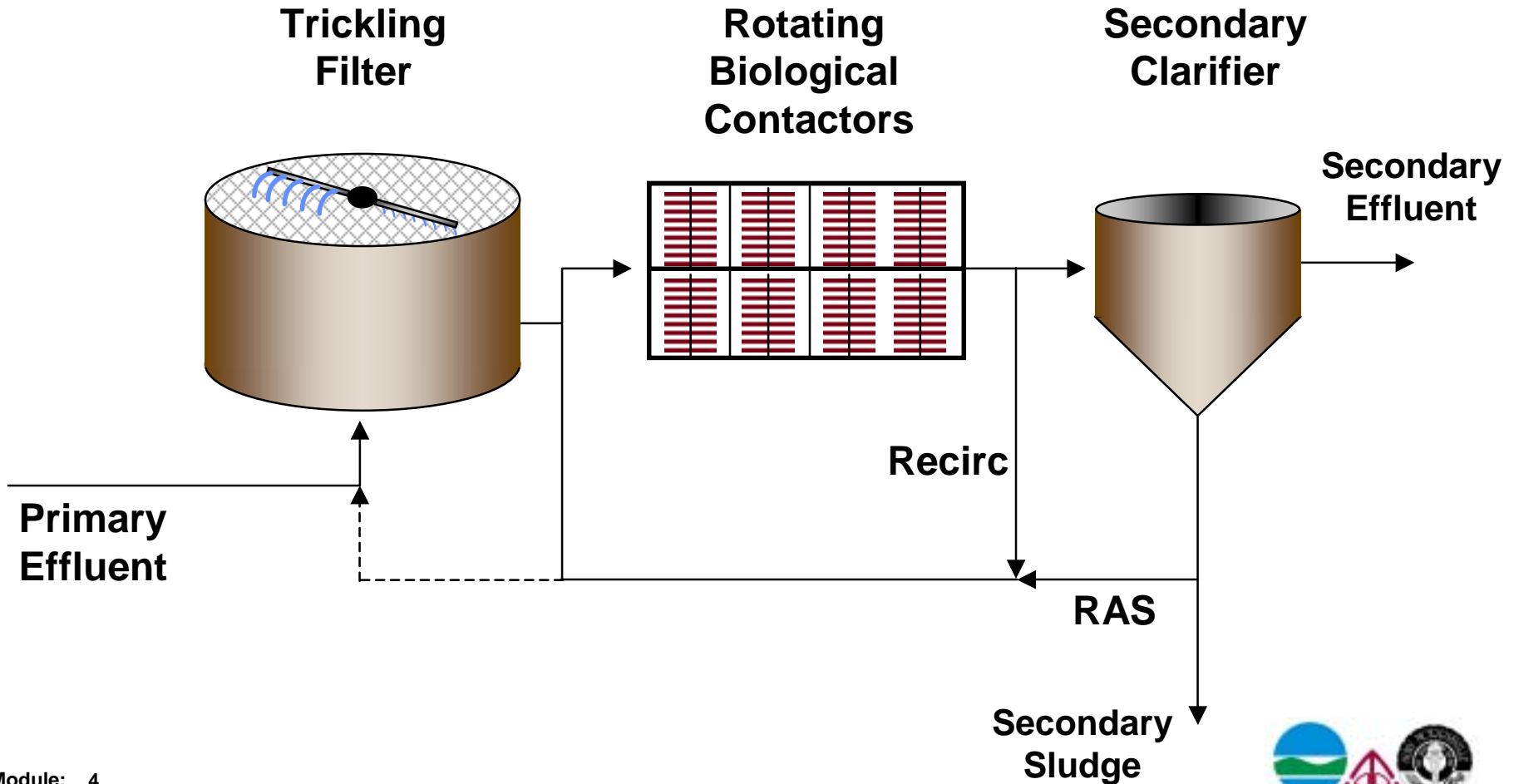
**Should First Stage Filters for BOD Removal Also Use Plastic Media?**

**How Thick Should the Biofilm Be?**

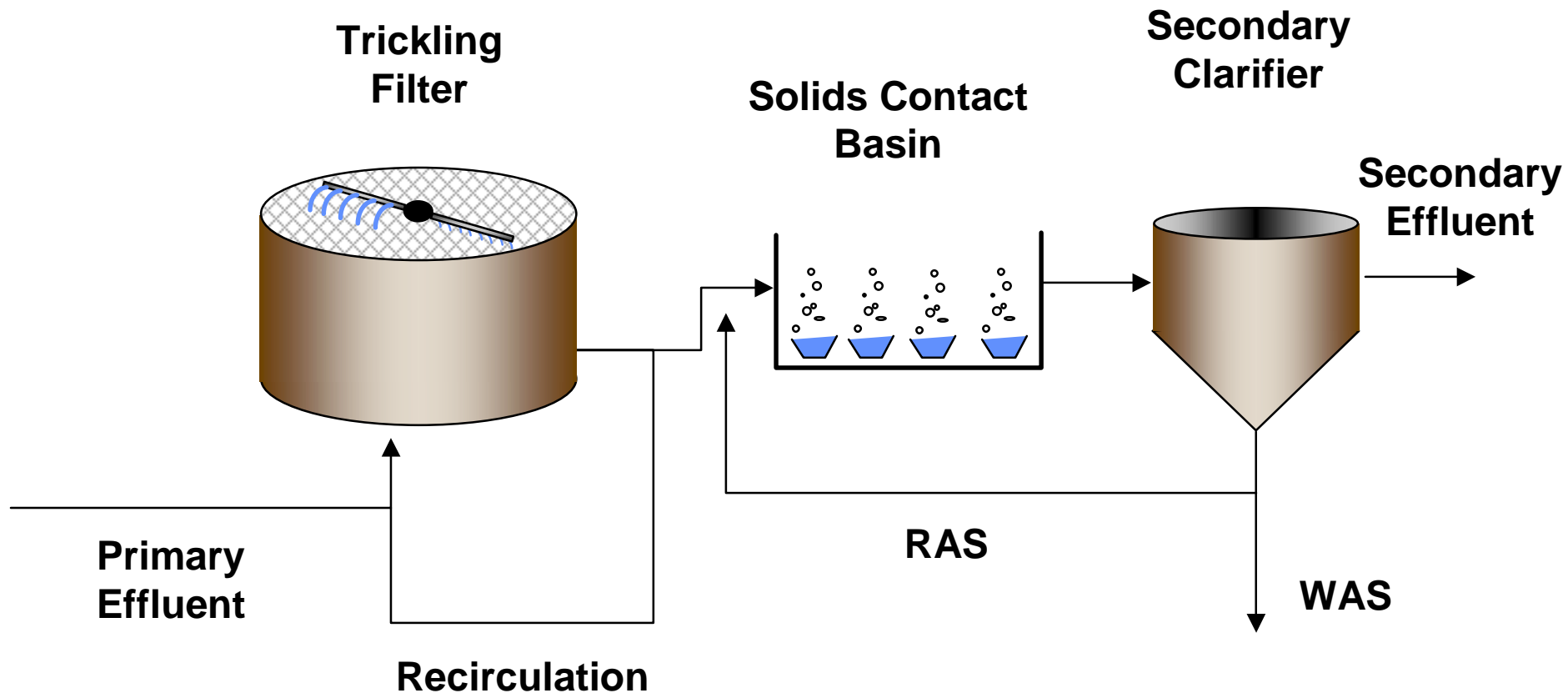
**How Do We Control Thickness?**



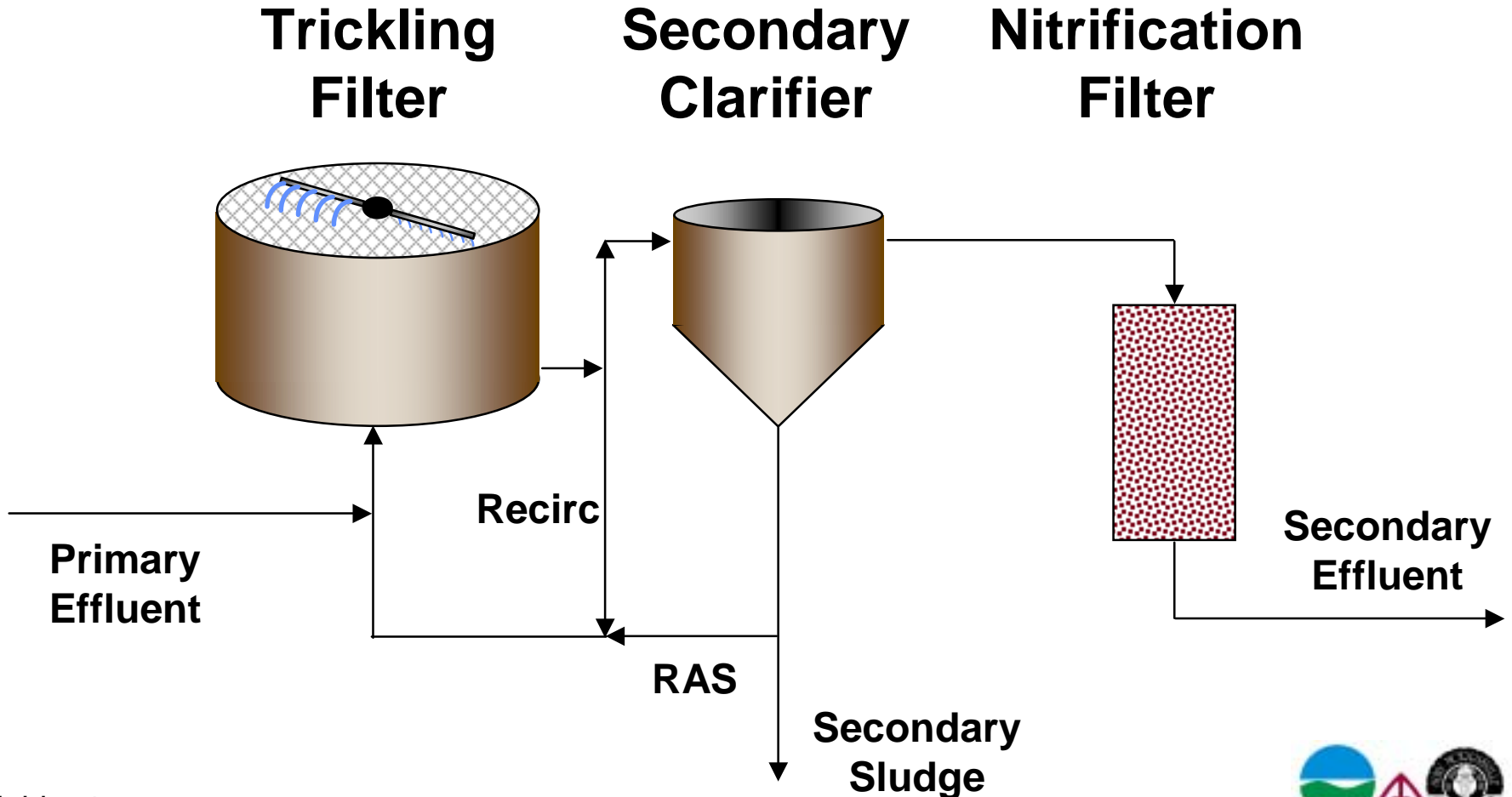
# *Trickling Filter Followed by RBCs*



# *Trickling Filter Solids Contact Process*



# *Trickling Filter Followed by Nitrifying Filter*





# *Evaluation of TF or RBC Loading Rate*

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- **Determine specific surface area of media**
- **Determine total surface area of media**
- **Determine BOD<sub>5</sub> loading rate**
- **Compare loading rate to standard rates**



# *Determine Specific Surface Area*

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- **Rock media (1" - 3")** **19 ft<sup>2</sup>/ft<sup>3</sup>**
- **Rock media (2" - 4")** **14 ft<sup>2</sup>/ft<sup>3</sup>**
- **Surfpac X-Flo 30** **30 ft<sup>2</sup>/ft<sup>3</sup>**
- **Surfpac X-Flo 42** **42 ft<sup>2</sup>/ft<sup>3</sup>**
- **Brentwood Accu-Pac CF-3000** **31 ft<sup>2</sup>/ft<sup>3</sup>**
- **Brentwood Accu-Pac CF-1900** **48 ft<sup>2</sup>/ft<sup>3</sup>**
- **Brentwood Accu-Pac CF-1200** **69 ft<sup>2</sup>/ft<sup>3</sup>**
- **See manufacturer's data sheet for other manufactured media**



# *Determine Total Media Surface Area*

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**Total Media Area (ft<sup>2</sup>) =**

**Specific Surface  
Area (ft<sup>2</sup>/ft<sup>3</sup>)**

**X**

**Total Media  
Volume (ft<sup>3</sup>)**



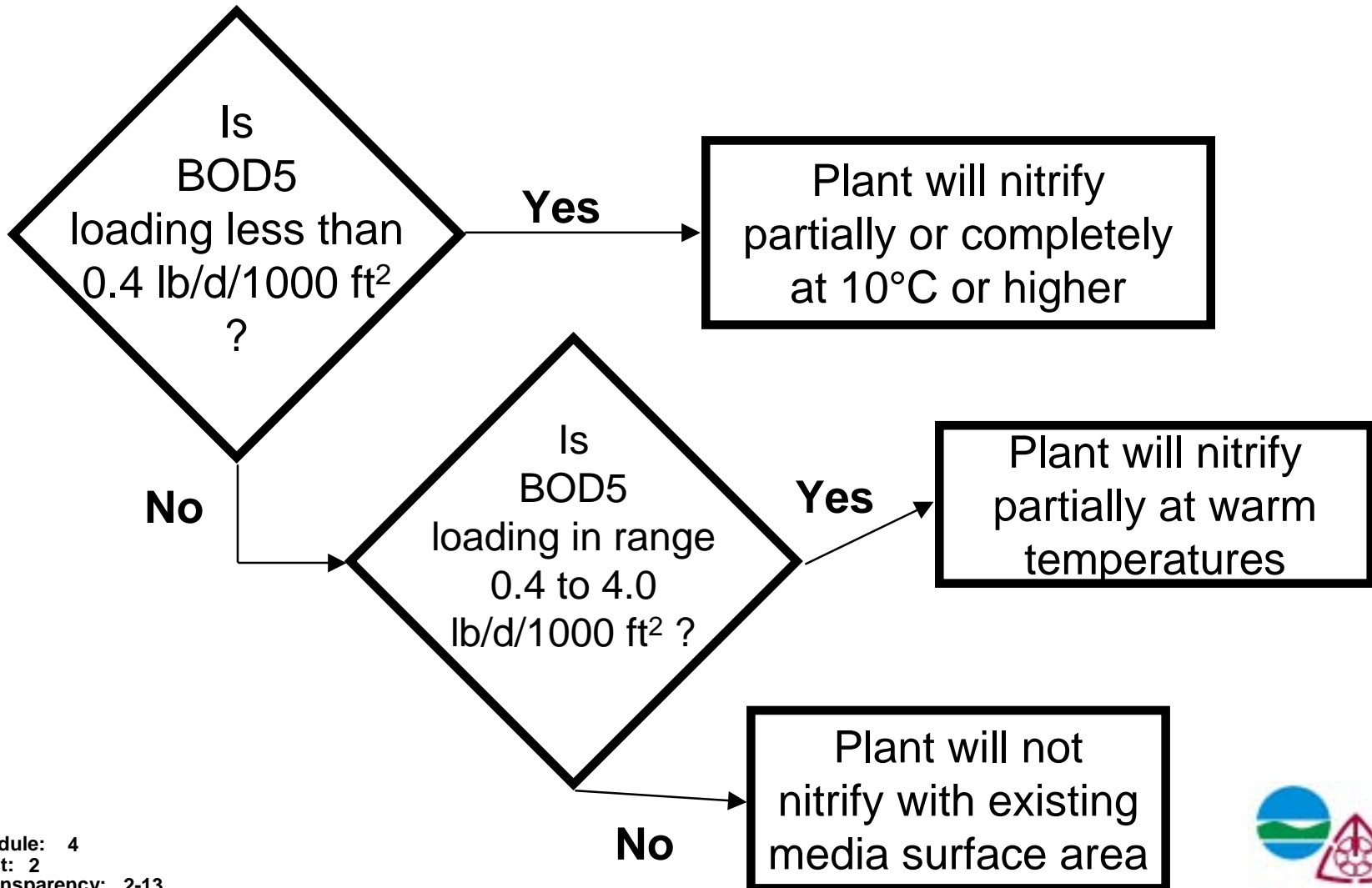
# *Determine BOD<sub>5</sub> Loading Rate*

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$$\text{BOD}_5 \text{ Loading Rate (lbs/1000 ft}^2\text{/day)} = \frac{\text{TF or RBC Influent BOD}_5 \text{ (lbs/d)}}{\text{Total Media Surface Area (1000 ft}^2\text{)}}$$



# *Evaluate Loading Rate*



# *Trickling Filter Media Replacement*

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**See worksheet**



# *Methods to Increase Dissolved Oxygen*

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- **Provide forced ventilation for trickling filters**
- **Increase hydraulic loading rate in trickling filters**
- **Replace trickling filter media with media with a greater void ratio**
- **Add diffused air in RBCs**



# *Biological Aerated Filters*

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- **Can be used as an add-on nitrifying filter when existing process cannot be made to nitrify**
- **Upflow or downflow configuration**
- **Various media including sand, shale, polystyrene**





# *Operating for Denitrification*

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**Now that my plant is nitrifying,  
what do I need to do to make it  
denitrify**



# *Operating for Denitrification*

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**Now that my plant is nitrifying,  
what do I need to do to make it  
denitrify**



**Establish anoxic conditions  
somewhere in the biological  
process.**



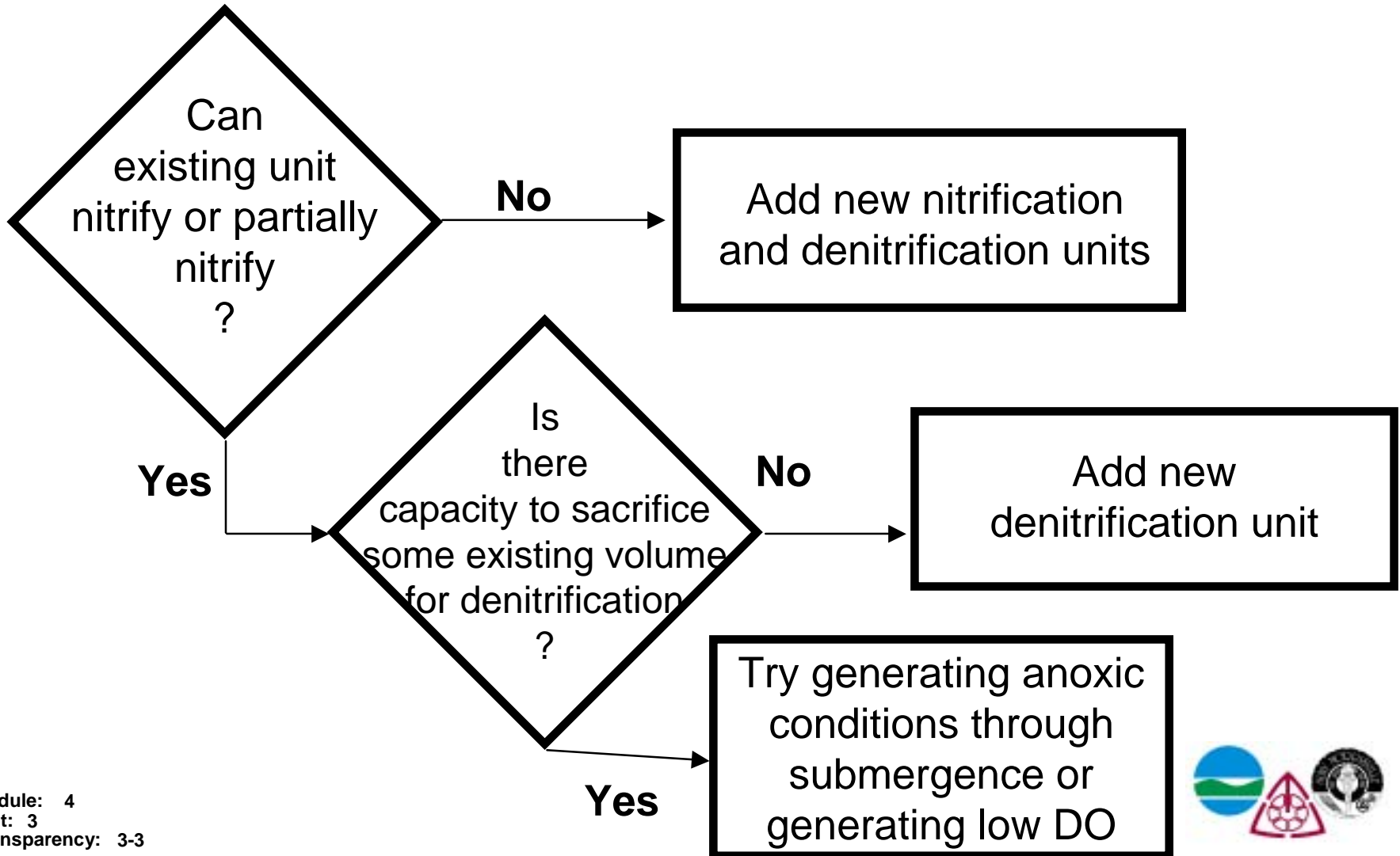
# *Methods to Achieve Denitrification*

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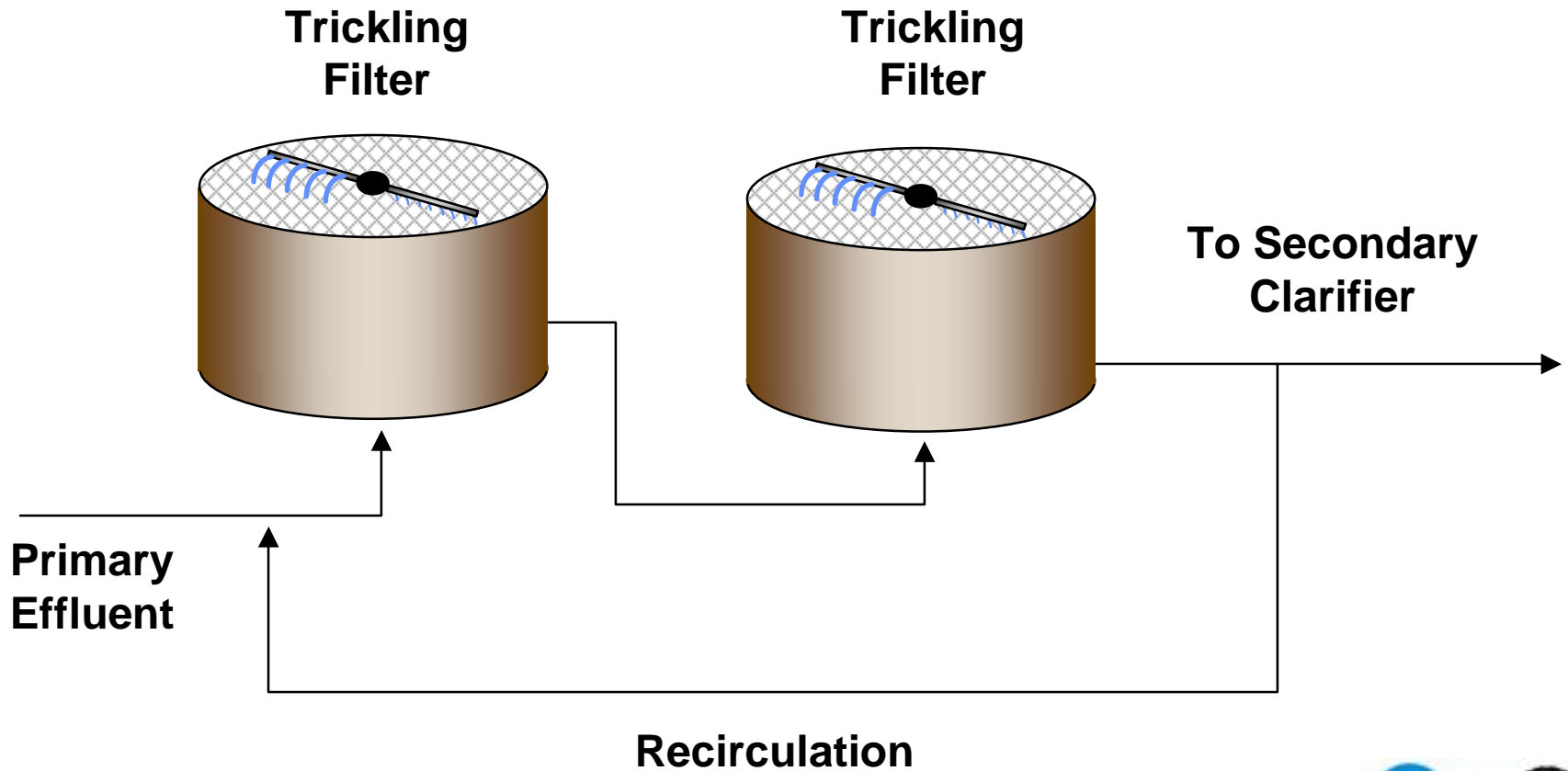
- **Incidental denitrification in trickling filter or RBC with recycle**
- **Convert a portion of existing unit to anoxic zone**
- **Add a new denitrification filter downstream of the nitrifying process**



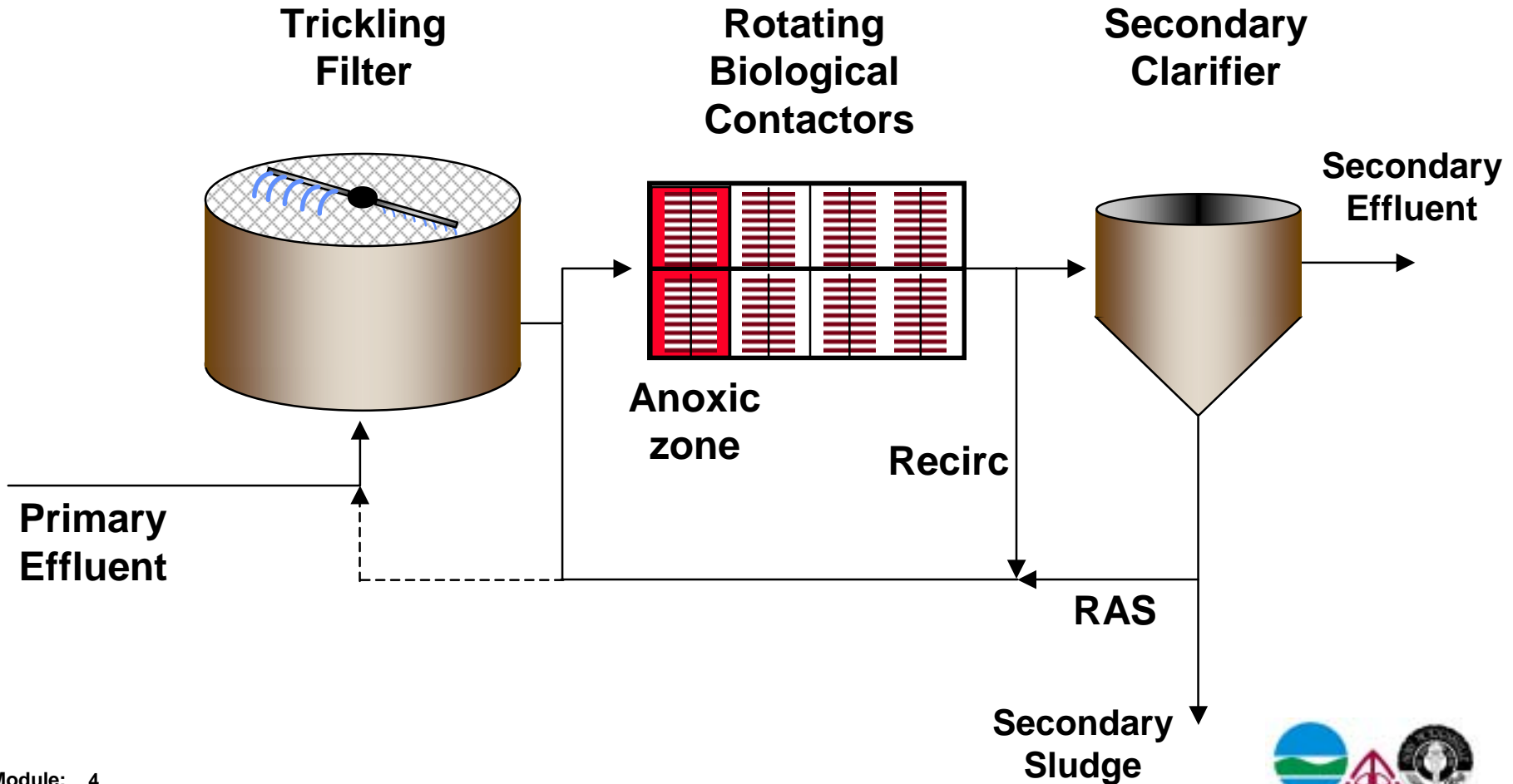
# *Preliminary Evaluation of Denitrification Alternatives*



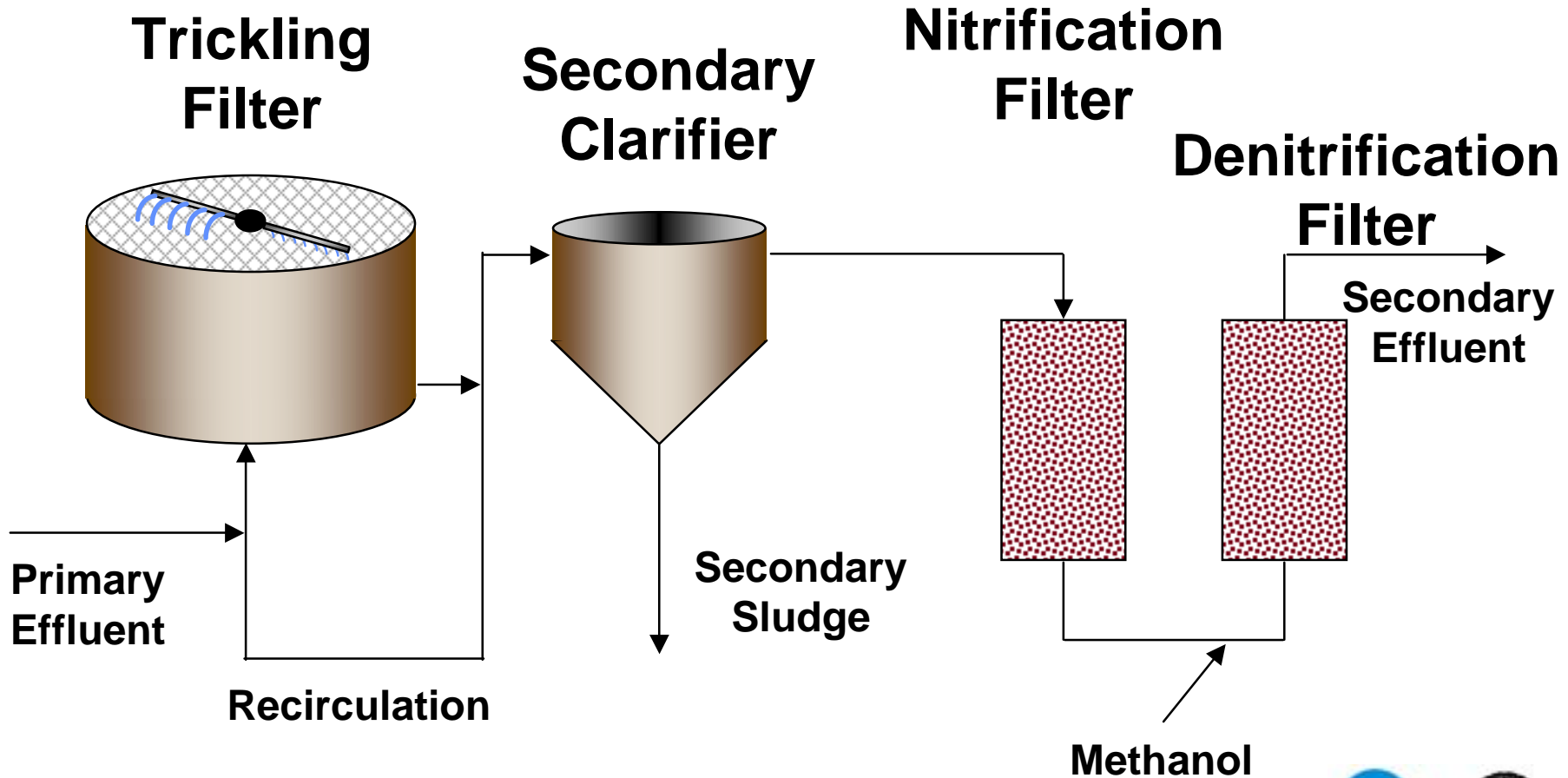
# *Incidental Denitrification*



# *Establishing an Anoxic Zone*



# *Trickling Filter Followed by Nitrifying and Denitrifying Filters*



# *Denitrification Filters*

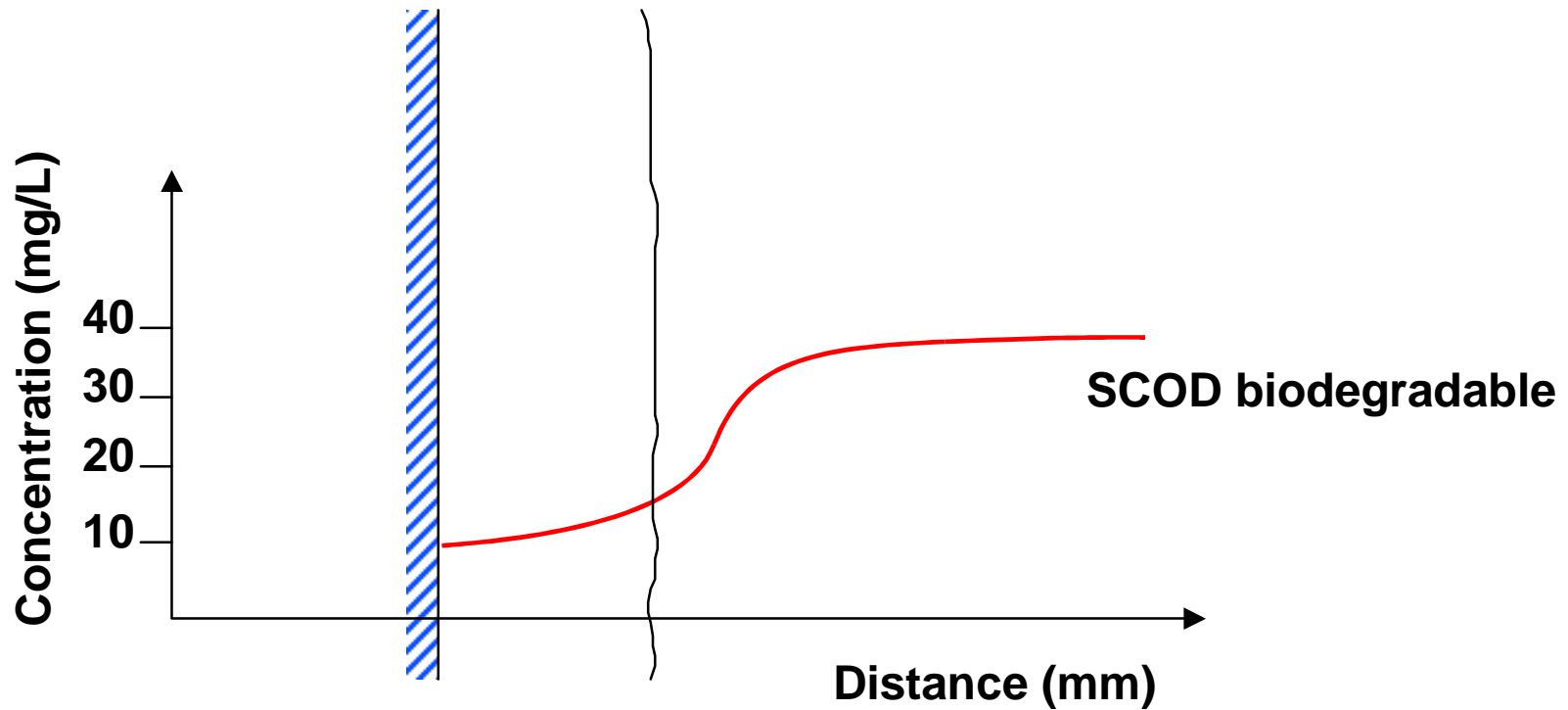
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- **Can be used as an add-on denitrifying filter when existing process cannot be made to denitrify**
- **Upflow or downflow configuration**
- **Various media including sand, shale, polystyrene**
- **Methanol addition for carbon source**

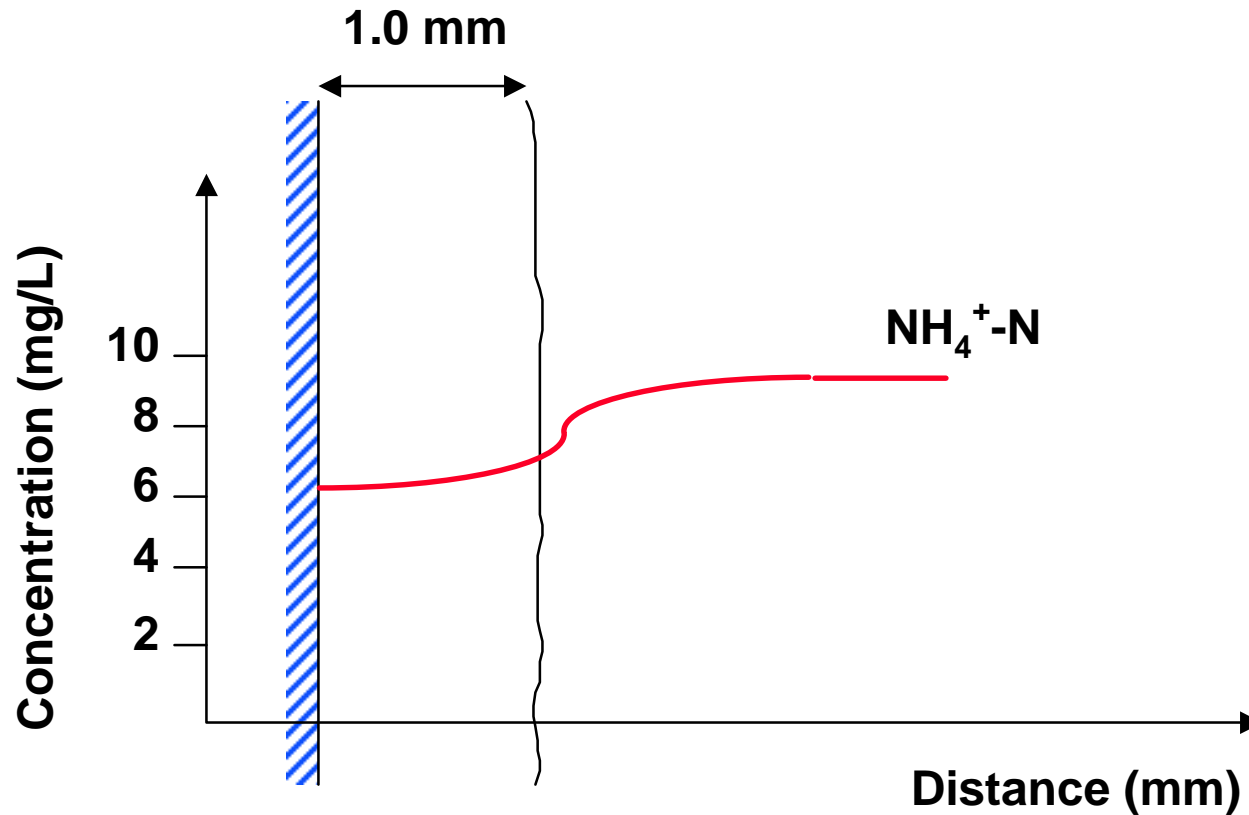




# *COD Depletion in Biofilm*

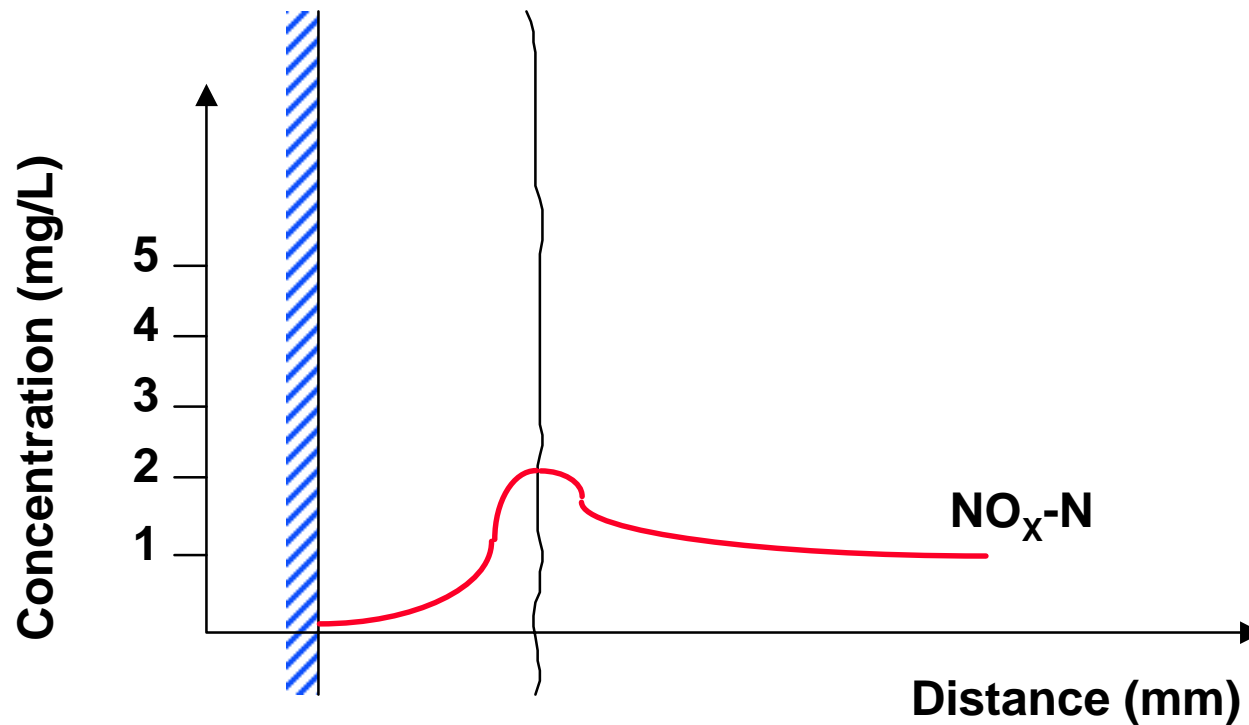


# Ammonia Depletion in Biofilm

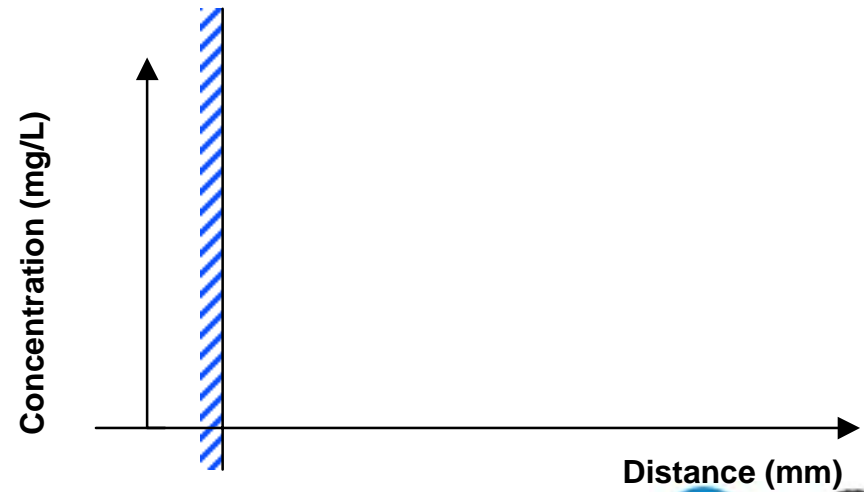
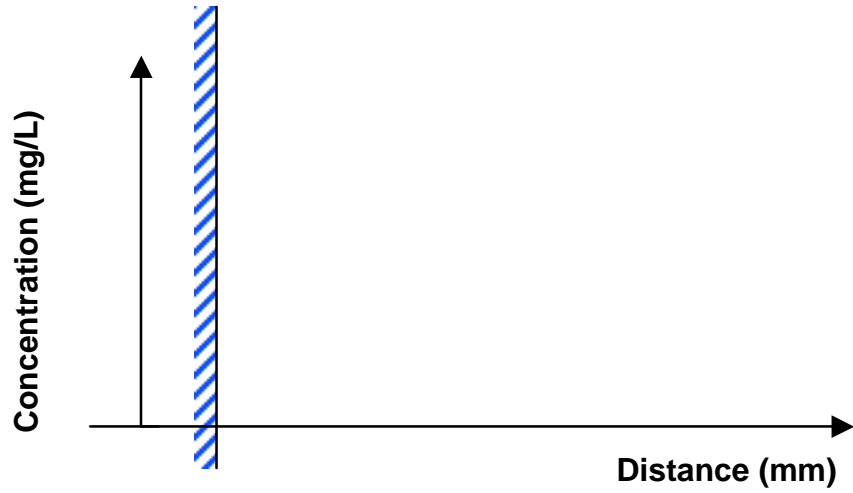


# *Nitrate Profile in Biofilm*

**Biofilm with some Nitrification**



# Biofilm Profiles



# *Fixed Film Discussion*

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- **Contact Between Biofilm Surface and Liquid Flowing Through the Filter.**
  - How Good Is the Contact?
  - Is It One Form?
  - How Do We Improve It?
- **Thickness of Stagnant Liquid Layer**
  - Should We Reduce Thickness?
  - How Is Biofilm Sloughing Affected?
- **Thickness of Biofilm**
  - A. Submerged Filters Vs. “Exposed to Air Filters”
  - B. Upflow Vs. Downflow

